



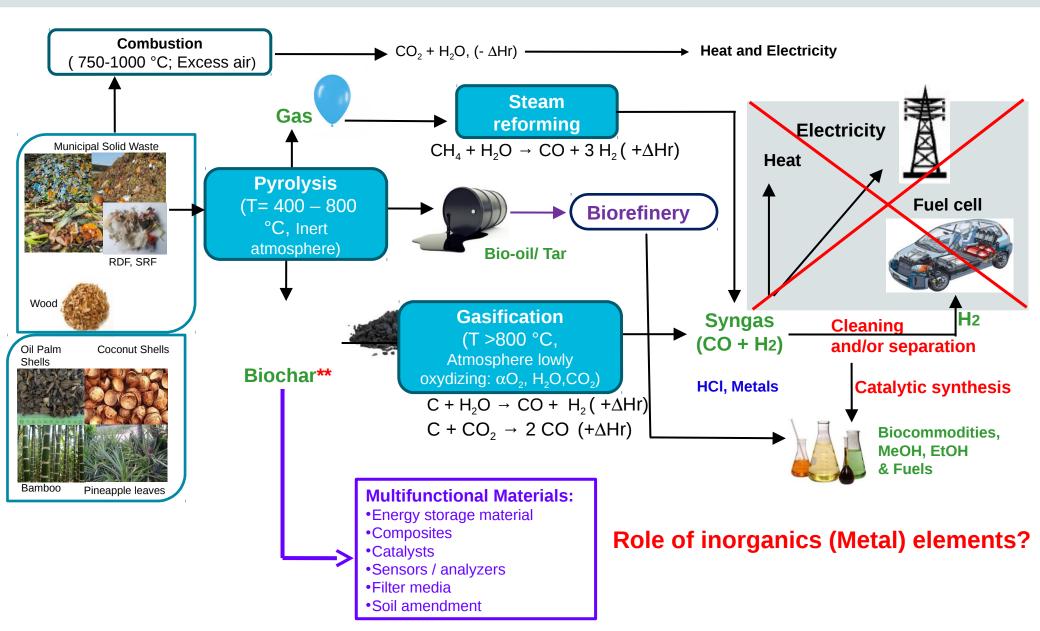
The catalytic effect of inherent and adorbed metals on the pyrolysis and gasification of biomass

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Waste and Biomass to VALUE (Energy and Valuable Materials)



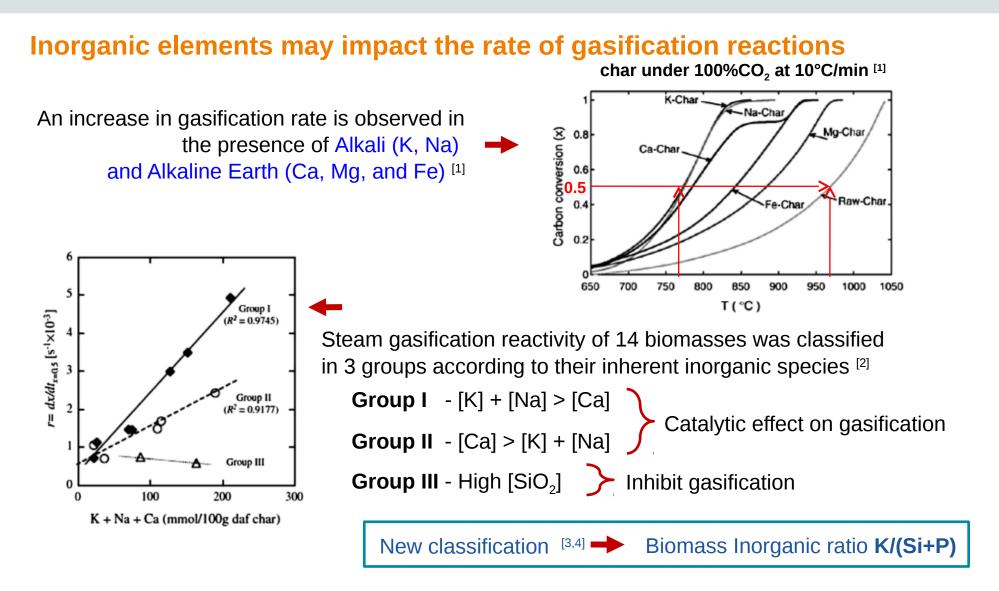
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OUTLINE

- **1.** Context
- **2.** Gasification experiments
- **3.** Results and discussion
- 4. Take to home



1. Context: State of the art – Gasification mechanisms



[1] Huang et al. Biotechnol Adv, 2009, 27; [2] Zhang W. Fuel Process Technol, 2010, 91;

[3] Romero M. at al, Fuel, 2019, 235; [4] Dupont C et al, Energy, 2016;

2. Gasification experiments: selection of biomass

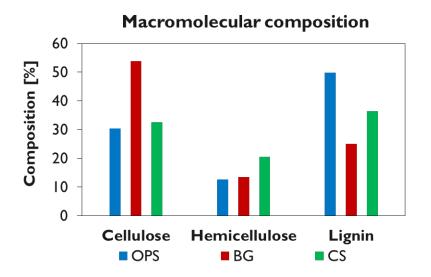
Steam gasification experiments of three different Agrowastes



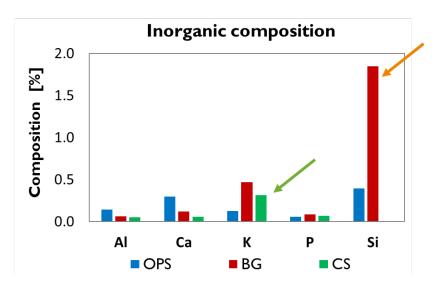
Composition and heating value		Oil Palm Shells	Coconut Shells	Bambou guadua
Elemental Analysis	С	46.7±0.2	46.8 ±0.2	42.7±0.3
(wt. % daf)	Н	6.5±0.1	5.8 ±0.1	5.4±0.1
	0	46.2±0.1	47.1 ±0.1	51.5±0.1
	N	0.6±0.1	0.3 ±0.1	0.4±0.1
	O/C	0.7±0.1	0.7±0.1	0.9±0.1
	H/C	1 7+0 1	1 5+0 1	1 5+0 1
Proximate analysis	Volatile Matter	69.9±0.3	71.4±0.3	68.3±0.2
(wt. %)	Fixed Carbon	19.0±0.3	17.1±0.2	18.1±0.3
	Ash	1.6±0.2	1.3±0.1	5.6±0.4
Heating value (MJ/kg) dry basis.	HHV	19.6±0.3	18.7±0.3	18.1±0.4

2. Gasification experiments: selection of biomass

Agrowastes



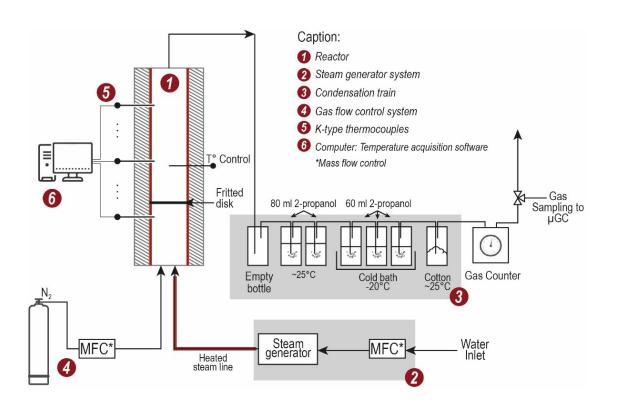
- Oil palm shells (OPS) and Coconut shells (CS) are endocarps with high lignin content
- Bamboo guadua (BG) is mainly composed of cellulose



- **Si, K** is the most important inorganic constituents of Bamboo guadua (BG)
- K is the most important inorganic constituent of Coconut shells (CS)

2. Gasification experiments

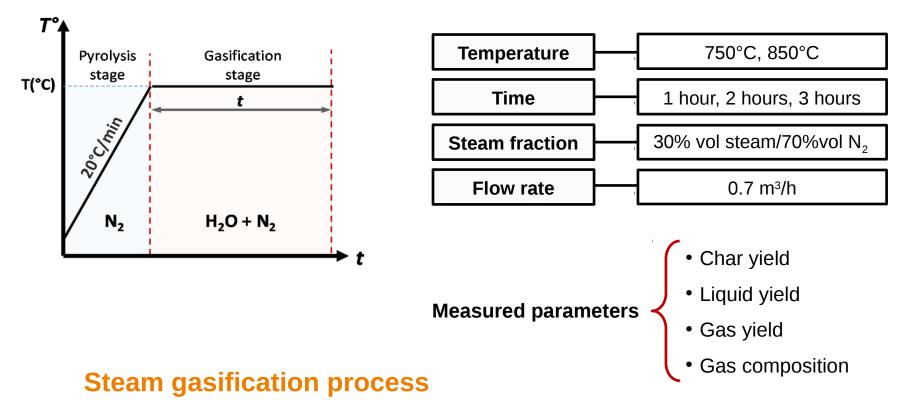
Experimental setup





Semi-continuous fluidized bed H: 60 ੴA? ☞ = 6 cm Raw biomass: 80 g Particle size: 2-3 mm

Experimental conditions and protocol



Experimental conditions

3. Results and discussion

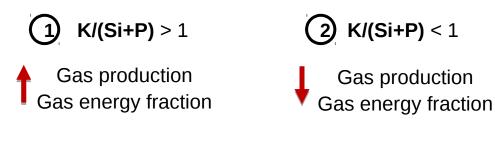
Energy distribution in the gasification products

Biomass composition impacts the product energy distribution:

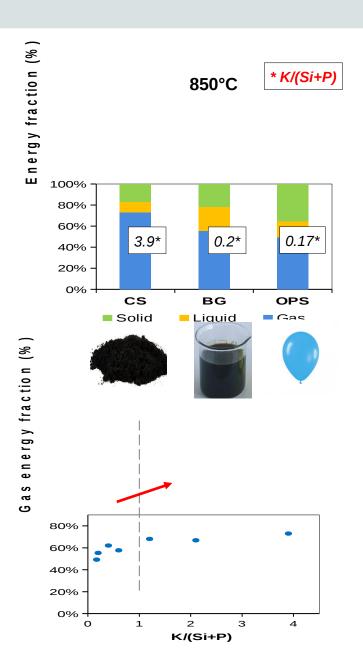
Product yield (%) = $\frac{m_{product}}{m_{biomass} + m_{steam}} x \ 100$

$$\begin{split} E_{products} &= E_{solid} + E_{gas} + E_{liquid} \\ E_{gas} &= m_{gas} \left(h_{gas \ (T_r)} + HHV_{gas} \right) \\ E_{liquid} &= m_{steam} \left(h_{steam \ (T_r)} \right) + m_{tars} \left(h_{tars \ (T_r)} + HHV_{tars} \right) \\ E_{solid} &= m_{char} \left(C_{p \ char} T_r + HHV_{char} \right) \end{split}$$

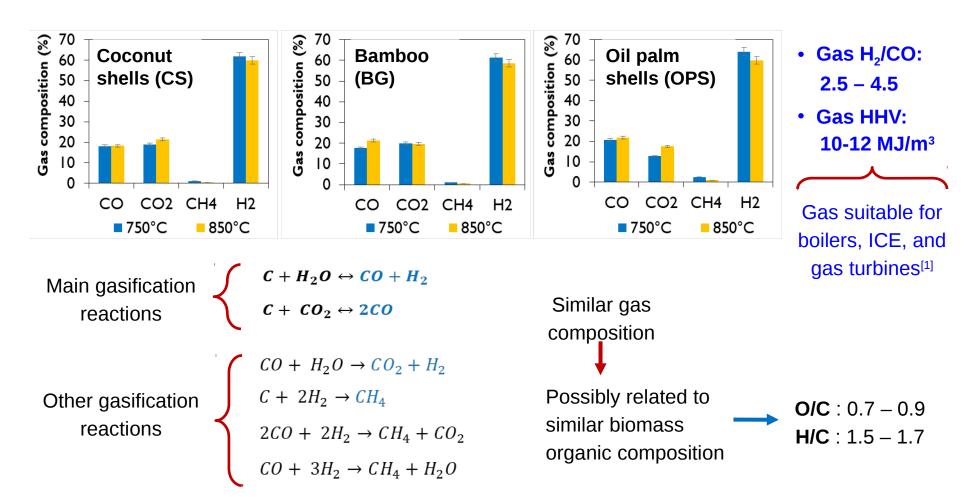
Under the same gasification conditions:



K/(Si+P) > 1 are associated with higher gasification
reactivities and process efficiencies



Gas composition and heating value



Results and discussion

Impact of biomass composition on the gasification behavior

Catalytic impact of AAEM* Oxygen transfer mechanism via the metal M^[1,2] on gasification reactions *AAEM: Alkali and Alkaline Earth Metal

Explaining water gas reaction mechanisms :

 $C + H_2 O \rightarrow CO + H_2$

Alkali metals (K, Na)	Alkaline earth metals (Ca, Mg)	H ₂	
$M_2CO_3 + 2C \rightarrow 2M + 3CO$	$MCO_3 + 2C \rightarrow M + 3CO$	→ M₂CO₃ + C	
$2M + 2H_2O \rightarrow 2MOH + H_2$	$M + 2H_2O \rightarrow M(OH)_2 + H_2$		
$2MOH + CO \rightarrow M_2CO_3 + H_2$	$M(OH)_2 + CO \rightarrow MCO_3 + H_2$		
	+ ($CO = 2 C + 2 H_2 O = 2 CO + 2 H_2$	

Explaining Boudouard reaction mechanism: **

 $C + CO_2 \rightarrow CO$

Alkali metals	Alkali
$M_2CO_3 + 2C \rightarrow 2M + 3CO$	MCO ₃
$2M + CO_2 \rightarrow M_2O + CO$	M + CC
$M_2O + CO_2 \rightarrow M_2CO_3$	MO + 0

line earth metals $+ 2C \rightarrow M + 3CO$ $O_2 \rightarrow MO + CO$ $CO_2 \rightarrow MCO_3$



Metal (M) loop

oxygen transfer

MOH

Η,

Syngas

 $+ H_2O$

3. Results and discussion

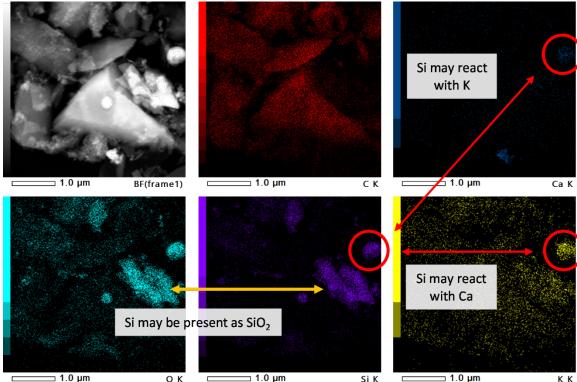
Impact of biomass composition on the gasification behavior

AAEM

AAEM* Catalytic effect inhibition

*AAEM: Alkali and Alkaline Earth Metal

Steam gasification biochar TEM-EDX cartography images



Formation of alkali phosphates, silicates and aluminosilicates [1-3]

M reactions with P, Si, Al

Inhibits the oxygen transfer mechanism via the metal M and its catalytic effect

Water gas reaction inhibition mechanism:

 $\boldsymbol{C} + \boldsymbol{H}_2 \boldsymbol{O} \rightarrow \boldsymbol{C} \boldsymbol{O} + \boldsymbol{H}_2$

Alkali metals (K, Na)

$$M_{2}CO_{3} + 2C \rightarrow 2M + 3CO$$

$$2M + 2H_{2}O \rightarrow 2MOH + H_{2}$$

$$2MOH \pm CO \rightarrow M_{2}CO_{3} + H_{2}$$

$$2MOH + nSiO_{2} \rightarrow M_{2}O \cdot nSiO_{2} + H_{2}O$$

[1] Zhang et al, Fuel, 2008; [2] Y. Niu, et al, Prog. Energy Combust. Sci. 52 (2016) 1–61; [3] D. Nutalapati et al. Fuel Process. Technol. 88 (2007) 1044–1052.

- The **inorganic content** of biomass has an important impact on the steam gasification reactivity, product yield, and gasification efficiency
- The **beneficial effect** of **AAEM (Alkali and Alkaline Earth Metals)** on the gasification behavior was **confirmed**, as well as the **inhibitory effect** of **Si** and **P**
- The inorganic ratio K/(Si+P) is a suitable indicator for gasification reaction of lignocellulosic biomass



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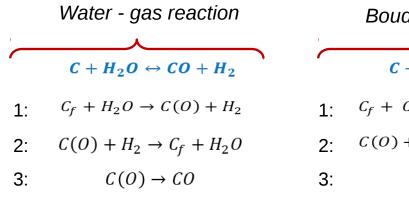






Deadline for abstracts submission: October 3, 2019

Main gasification reactions and mechanisms



	Boudouard reaction	
_		
	$C + CO_2 \leftrightarrow 2CO$	
.:	$C_f + CO_2 \to C(0) + CO$	
2:	$C(0) + CO \rightarrow C_f + CO_2$	
8:	$C(0) \rightarrow CO$	

Intermediate steps

[1,2]: Step 1: Dissociation of the reactant at a carbon-free active site (C_i)

- Step 2: Formation of a carbon-oxygen surface complex C(O)
- Step 3: Desorption of product species

Other gasification reactions

- Methanation reactions

- Water - gas shift reaction $\langle CO + H_2O \rightarrow CO_2 + H_2 \rangle$ Hydrogasification reaction $\langle C + 2H_2 \rightarrow CH_4 \rangle$ $2CO + 2H_2 \rightarrow CH_4 + CO_2$ $CO + 3H_2 \rightarrow CH_4 + H_2O$ $CO_2 + 4H_2 \rightarrow CH_4 + 2H_2O$